

Ionic Water Technologies

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Semi-Passive Bioreactors for Treatment of Acid Mine Drainage

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Bridging the Gap Between Passive and Active

PASSIVE Limestone channels Organic bioreactors		ACTIVE SAPPS Semi-Passive bioreactors RCTS Lime Treatment HDS RO
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Solubility Products for Metal Complexes

Complex	K_{sp}	Complex	K_{sp}
HgS	6.38 x 10 ⁻⁵³	Zn(OH)₂	7.68 x 10 ⁻¹⁷
Fe(OH)₃	2.67 x 10 ⁻³⁹	Ni(OH)₂	5.54 x 10 ⁻¹⁶
CuS	1.28 x 10 ⁻³⁶	Cd(OH)₂	5.33 x 10 ⁻¹⁵
CdS	1.4 x 10 ⁻²⁹	MnS	4.55 x 10 ⁻¹⁴
PbS	8.81 x 10 ⁻²⁹	Mn(OH)₂	2.04 x 10 ⁻¹³
ZnS	2.91 x 10 ⁻²⁵	PbCO₃	1.48 x 10 ⁻¹³
NiS	1.08 x 10 ⁻²¹	CdCO₃	6.20 x 10 ⁻¹²
Pb(OH)₂	1.4 x 10 ⁻²⁰	FeCO₃	3.13 x 10 ⁻¹¹
FeS	1.57 x 10 ⁻¹⁹	MnCO₃	2.23 x 10 ⁻¹¹
Fe(OH)₂	4.79 x 10 ⁻¹⁷	NiCO₃	1.45 x 10 ⁻⁷

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Treatment Process Sulfate-reducing Bioreactors

Sulfate-reduction

$$4 \text{AH}_2 + \text{SO}_4^{2-} + 2 \text{H}^+ \rightarrow 4 \text{A}^{2+} + \text{H}_2\text{S} + 4 \text{H}_2\text{O}$$

Ethanol + Sulfate + Acidity \longrightarrow Carbon Dioxide + Hydrogen sulfide + Water

Sulfide Precipitation of Metals

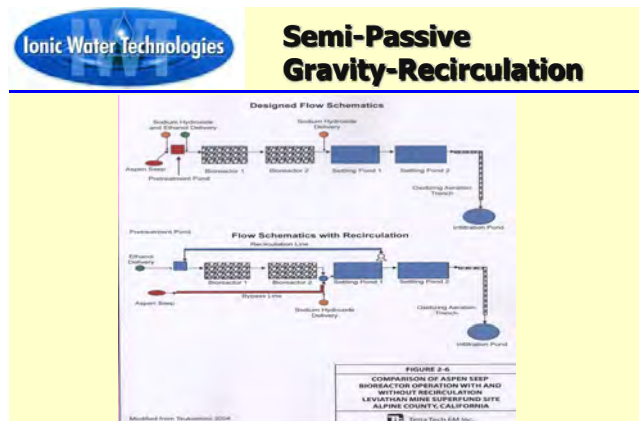
$$\text{H}_2\text{S} + \text{M}^{2+} \rightarrow \text{MS} + 2 \text{H}^+$$

Hydrogen sulfide + Metals \longrightarrow Metal sulfides

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Organic Substrates for Sulfate Reducing Bacteria

<ul style="list-style-type: none"> • Formate • Acetate • Lactate • Pyruvate • Malate • Fumarate • Succinate • Alkanes • Various sugars • Glycerol 	<ul style="list-style-type: none"> • Methanol • Ethanol • Propanol • Butanol • Ethylene glycol • Propane diol • Benzoate • Phenols (many types) • Others
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Rock vs. Organic Substrate

<u>Parameter</u>	<u>Rock</u>	<u>Organic</u>
Food Source Built in	No	Yes
External Food Supply	Yes	Optional
Flushable	Optional	No
Gravity Mode	Yes	Yes
Recycle Mode	Yes	Yes
Substrate Needs Replacement	No	Yes

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Rock vs. Organic Substrate

<u>Parameter</u>	<u>Rock</u>	<u>Organic</u>
<input type="checkbox"/> Bed Depth Limited	No	Yes
<input type="checkbox"/> Prone To Short Circuits	No	Yes
<input type="checkbox"/> Requires Rebuilding	No	Yes
<input type="checkbox"/> Complex Microbial Culture	No	Yes
<input type="checkbox"/> Quick Response to Controls	Yes	No
<input type="checkbox"/> Requires constant food addition	Yes	No

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Gravity vs. Recycle

	<u>Gravity Flow</u>	<u>Recycle Flow</u>
<input type="checkbox"/> Rock Substrate	Yes	Yes
<input type="checkbox"/> Organic Substrate	Yes	Yes
<input type="checkbox"/> Low pH Water	Pretreat	Yes
<input type="checkbox"/> Toxic Metal Levels OK	No	Yes
<input type="checkbox"/> Requires Power	No	Yes
<input type="checkbox"/> Precipitate Outside Reactor	No	Yes
<input type="checkbox"/> Precipitate May Clog Reactor	Yes	No
<input type="checkbox"/> Extended Life	No	Yes
<input type="checkbox"/> May Require Pretreatment	Yes	No

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Leviathan Bioreactors



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- Built fall 2002 – Spring 2003
- Pretreat by raising pH over 4
- 2 rock SRB cells
- 1 pretreat and 2 post treat ponds
- Design flow 20-30 gpm, Peak 40 gpm
- Average flow Aspen Seep 12 gpm
- Status – met targets-replaced by recycle
- Climate – cool (snow in April)
- SRB residence time at 10 gpm is 100 HRS



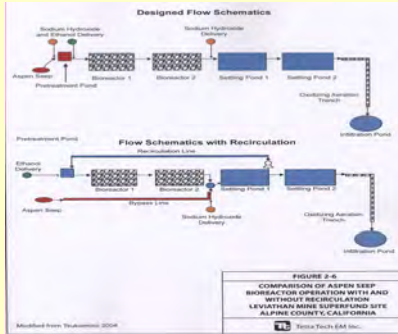
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Leviathan Bioreactor Pretreat with Sodium Hydroxide :Precip Al & Fe 2003



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Comparison Gravity-Recirculation



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 New 2010 2010

Table 2. Bioreactor Treatment System Removal Efficiencies: Gravity Flow Configuration

Target Metal	Number of Sampling Events	Average Filtered Influent Concentration (µg/L)	Standard Deviation	Average Filtered Effluent Concentration (µg/L)	Standard Deviation	Exceeds Discharge Standard (Y/N)	Average Removal Efficiency (%)	Range of Removal Efficiencies (%)
Primary Target Metals								
Aluminum	6	37,467	2,011	103	78.8	N	99.7	99.5 to 99.9
Arsenic	6	2.1	0.64	4.7	4.0	N	NC	NC
Copper	6	691	51.2	4.8	1.6	N	99.3	99.1 to 99.7
Iron	6	117,167	6,242	4,885	4,771	Y	95.8	65.6 to 99.9
Nickel	6	487	33.5	65.5	36	N	86.6	72.1 to 92.6
Secondary Target Metals								
Cadmium	6	0.61	0.27	<0.21	0.07	N	65.3	42.5 to 79
Chromium	6	12.2	8.9	7.8	6.6	N	NC	NC
Lead	6	3.6	2.5	4.7	2.9	N	NC	NC
Selenium	6	13.9	3.1	11.2	2.6	Y	NC	NC
Zinc	6	715	47.1	15.8	6.8	N	97.8	95.9 to 98.6

NC = Not calculated as influent and effluent concentrations were not statistically different
 µg/L = Microgram per liter

Constituent	Aspen Seep	Bioreactor 1 effluent	Bioreactor 2 effluent	Discharge	Discharge objectives
pH	3.17	4.70	4.77	7.19	6-9
SO ₄	1502	1307	1269	1222	NA
Al	35	21	18	<0.1	4.0
Fe	107	69	65	1.9	2.0
Ni	0.40	0.26	0.21	0.06	.84
Cu	0.55	0.01	<0.01	<0.01	.026
Zn	0.74	0.08	0.04	0.02	.21





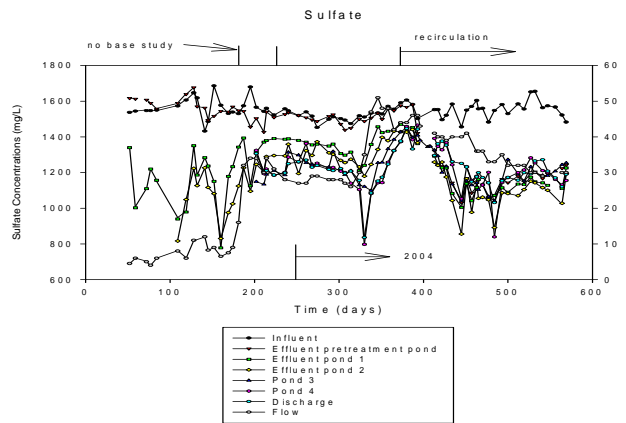
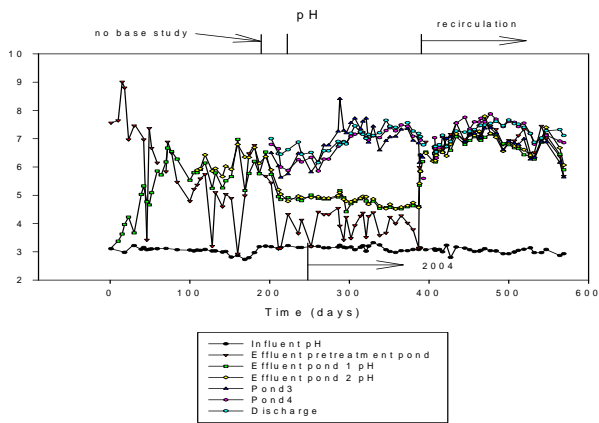
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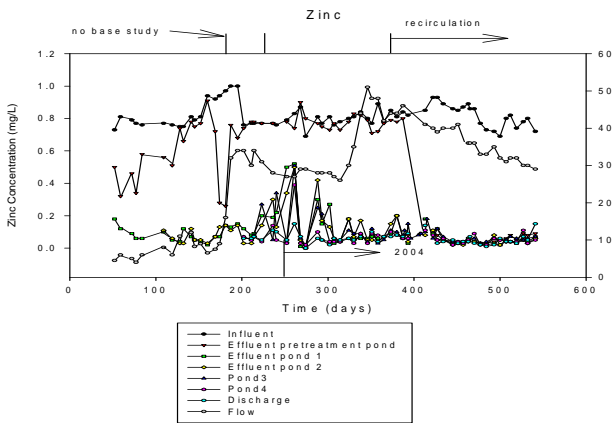
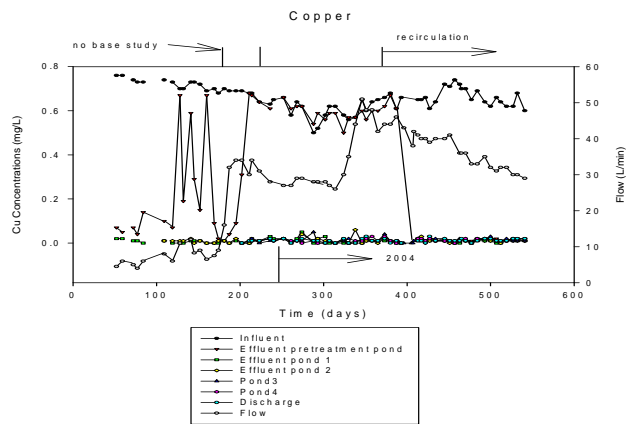
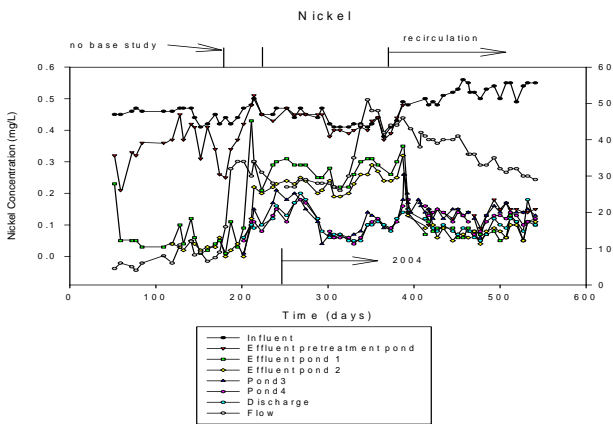
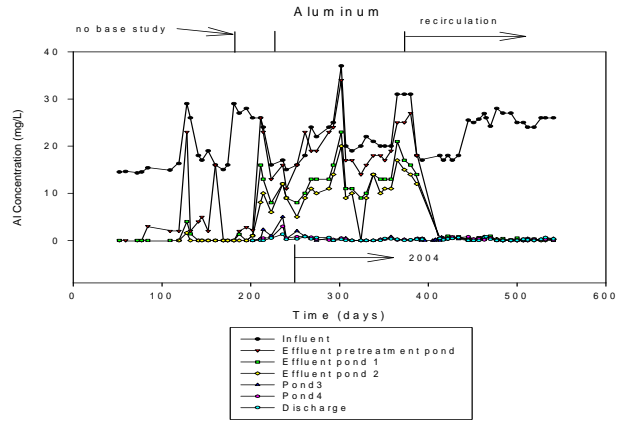
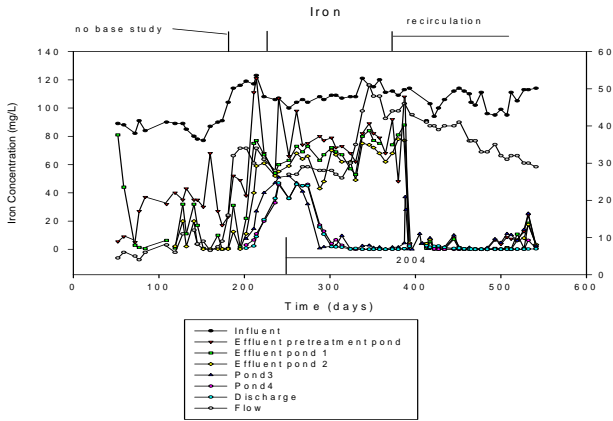
Table 3. Bioreactor Treatment System Removal Efficiencies: Recirculation Configuration

Target Metal	Number of Sampling Events	Average Filtered Influent Concentration (µg/L)	Standard Deviation	Average Filtered Effluent Concentration (µg/L)	Standard Deviation	Exceeds Discharge Standard (Y/N)	Average Removal Efficiency (%)	Range of Removal Efficiencies (%)
Primary Target Metals								
Aluminum	7	40,029	4,837	52.7	25.7	N	99.9	99.7 to 99.9
Arsenic	7	7.4	6.5	6.5	4.9	N	NC	NC
Copper	7	795	167	4.6	3.2	N	99.4	98.8 to 99.8
Iron	7	115,785	13,509	2,704	3,000	Y	97.7	92.8 to 99.7
Nickel	7	529	34.1	69.7	44.2	N	86.8	71.0 to 96.4
Secondary Target Metals								
Cadmium	7	0.60	0.50	<0.20	0.09	N	NC	NC
Chromium	7	11.1	6.3	6.4	5.2	N	42.5	21.2 to 84.8
Lead	7	4.2	2.3	2.5	1.6	N	41.5	22.8 to 57.1
Selenium	7	11.5	5.1	8.5	3.6	Y	NC	NC
Zinc	7	776	51.7	8.9	7.4	N	98.9	97.7 to 99.8

NC = Not calculated as influent and effluent concentrations were not statistically different
 µg/L = Microgram per liter

Constituent	Aspen Seep	Bioreactor 1 effluent	Bioreactor 2 effluent	Discharge	Discharge objectives
pH	2.93	6.79	6.86	7.66	6-9
SO ₄	1530	1090	1080	1170	NA
Al	28	<0.5	<0.5	<0.5	4.0
Fe	99	0.16	0.13	0.04	2.0
Ni	0.50	0.15	0.05	0.1	0.84
Cu	0.62	0.02	0.01	0.01	0.026
Zn	0.73	0.02	0.02	0.06	0.21





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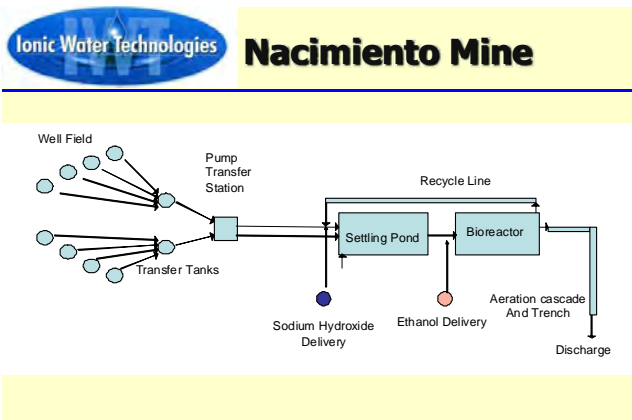
Residence Time and Working Volume for Leviathan Bioreactor

System Component	Working Volume	Calculated Residence Time (38 Lpm)
Pretreatment Pond	100 ft ³	0.5 days
Pond 1	5,300 ft ³	3.5 days
Pond 2	3,000 ft ³	1.5 days
Settling Pond 1	16,500 ft ³	8.5 days
Settling Pond 2	18,000 ft ³	9.4 days
Totals	42,900 ft³	23 days



Ionic Water Technologies **Nacimiento Mine**

US Forest Service New Mexico
Up to 120 gpm, Rock Substrate, Recycle
Construction Completed 2009



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Residence Time and Working Volume for Nacimiento Bioreactor

System Component	Working Volume	Calculated Residence Time (240 Lpm)
Settling Pond	117,000 ft ³	7.5 days
Bioreactor	50,000 ft ³	3.2 days
Totals	167,000 ft³	10.7 days

Ionic Water Technologies **Comparison Between Nacimiento and Leviathan**

Average Influent and Effluent Concentrations of Constituents of Concern (Dissolved Metals mg/L)

Sample Location	Number of sampling events	pH	Sulfate	Al	Cu	Fe	Ni	Zn
Leviathan Mine Influent*	7			40.0	0.795	116	0.529	0.776
				4.837**	0.187**	13**	0.034**	0.052**
Leviathan Mine Effluent*	7			0.0527	0.0046	2.704	0.0697	0.0089
				0.026**	0.003**	3.0**	0.044**	0.007**
Leviathan Discharge Objective*				4.000	0.026	2.000	0.840	0.210
Nacimiento Mine Influent	9	4.91	884	2.35	17.84	61.6	0.09	4.44
				1.83**	25.12**	0.041**	0.041**	2.239**
Nacimiento Mine Effluent	9	6.89	385	<0.05***	0.004	0.07	0.0032	0.0083
					0.002**	0.039**	0.001**	0.004**
Nacimiento Discharge Objective		6.6-8.8	NA	0.087	0.0152	NA	0.088	0.198

*Data from EPA 2006
 **Standard deviation
 *** 4 values detected all at less than 0.056 mg/l and an average concentration of .036 mg/L

Ionic Water Technologies **Choosing the System for Your Application**

Parameter	Organic	Rock	Gravity	Recycle
Life Span	5 years ?			20 Years +
pH below 3.5	---	---	Pretreat	OK
Fe over 1000 mg/L	---	---	Pretreat	OK
Al over 10 mg/L	---	---	Pretreat	OK
Power Available	---	---	Yes	OK
No Power	---	---	Yes	No
Microbe Toxicity	---	---	No	OK
Zn over 75 mg/L				
Cu over 5 mg/L				
Highly variable Flow Rate	---	---	No	Possible
Requires N Add	No	Yes	---	---
Requires C Add	No	Yes	---	---
No winter Access	OK	No	OK	No
Influent Oxidized	---	---	No	OK